

# Transferability of water calibration to energy-transition relevant fluids applications using Coriolis mass flowmeters

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## ABSTRACT

The results of a calibration round performed on Coriolis mass flowmeters, originally calibrated with water at factory conditions and recalibrated with different fluids at several flow calibration facilities, are discussed in this paper. These calibrations were dedicated to proving the transferability concept from water to other fluids, some of which are relevant to energy transition. The obtained results confirmed the robustness of the tested instruments' performance and the viability of using the transferability approach as a reliable alternative.

## Section: RESEARCH PAPER

**Keywords:** transferability; Coriolis mass flowmeter; energy transition

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## 1. INTRODUCTION

Metrological authorities and regulatory bodies have often discouraged the use of alternative fluids in flow calibrations because of the possible impact of fluid property variations, such as density and viscosity, on the flowmeter's performance. However, the use of advanced flow measurement technologies and the need to handle fluids with diverse properties and process conditions (some of which are associated with the energy transition era) have sparked the discussion about the transferability concept. This concept supports the use of alternative fluids, different from the process fluid for both the initial and subsequent calibrations of the flowmeters, providing a potential alternative to the conventional approach.

Coriolis mass flowmeters (CMFs) have been particularly involved in the application of the transferability concept. This technology has also been one of the first choices for measuring different fluids in applications such as custody transfer, but under challenging conditions, e.g., very low density, high viscosity, dense phase, or close to critical conditions. However, the performance of the flowmeter under these operational conditions must be proved by experimental means as well.

The results of a calibration round carried out on a group of CMFs, originally calibrated with water and then recalibrated without adjustments at several flow calibration facilities, using gas and high-viscosity fluids, are discussed in this paper. These calibrations were intended to prove the transferability concept from water to other fluids, relevant to the global energy transition strategy.

## 2. CORIOLIS MASS FLOWMETER PRINCIPLE OF OPERATION

The Coriolis mass flow measurement principle is based on the linear relationship between the mass flowing ( $q_m$ ) through the measuring tubes of the device and the phase shift ( $\Delta\phi$ ) or delay ( $\Delta t$ ) detected between two points (A and B in Figure 1) in the measuring tubes, equipped with electrodynamic sensors. Each measuring tube oscillates at its resonance frequency, imposed by the excitation driver. The phase shift ( $\Delta\phi$ ) is caused by the so-called Coriolis force, which is proportional to the mass flow rate ( $q_m$ ). CMFs can also measure fluid density and temperature.

Coriolis mass flowmeters can be initially calibrated using water as the calibration fluid, and the gravimetric approach as the calibration method, following the standard ISO 4185 [1]. Water

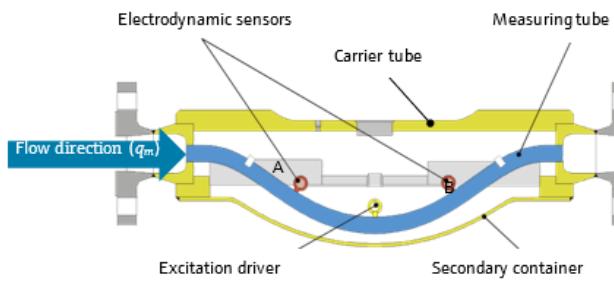


Figure 1. Coriolis sensor (simplified diagram).

calibration is a preferred approach that allows a consistent evaluation of flowmeter performance using a well-known fluid under reference conditions. The water used in the calibration process is filtered, and its density, as well as the content of solids, is measured and maintained within an acceptable range. Under these conditions, deviations can be identified, isolated, and corrected, thus the obtained calibration factor (CALF) properly represents the sensitivity of the meter.

Depending on the manufacturer and the meter characteristics, this CALF can also be valid for liquids other than water. This transferability or extension of the CALF validity to other fluids must be proved through experimental tests.

### 3. CORIOLIS MASS FLOWMETER IN GAS APPLICATIONS

Coriolis mass flowmeters show good performance in gas applications such as natural gas ( $\text{CH}_4$ ), compressed natural gas (CNG), as well as in diverse  $\text{H}_2$  and  $\text{CO}_2$  applications, including custody transfer. Gas applications are particularly stringent for Coriolis mass flowmeters due to the low density of the fluid, and, consequently, their operation in the lower region of the flowmeter mass flow range, where the zero point stability plays a relevant role. These flowmeters are designed with specific features allowing this effect to be reduced. Two examples of these features are the high homogeneity of the materials used to build these instruments and the strict symmetry tolerances allowed during their construction. These features help to balance the mechanical behaviour of the measuring tube's dynamic, thus reducing the impact on zero point stability.

However, gas flow measurement with CMF deals with the compressible behaviour and the low speed of sound (SoS) of the gas, responsible for introducing changes in the resonance frequency with respect to the driving frequency imposed on the measuring tubes. This gas-related frequency effect is mainly influenced by three elements: the SoS in the gas, the fluid velocity, and the measuring tube's geometry. These three elements are taken into consideration when implementing corrections to mitigate their effect.

AGA Report No. 11 API MPMS Chapter 14.9, section 7 [2] states: "Calibration with an alternative calibration fluid (e.g., water) is valid with Coriolis sensor designs where the transferability of the alternative calibration fluid, with an added uncertainty relative to gas measurement, has been demonstrated by the meter manufacturer through tests conducted by an independent flow calibration laboratory." This statement validates, in line with principle, the calibration results obtained in gas measurement with Coriolis mass flowmeters originally calibrated with water, whenever the new accuracy and uncertainty values are clearly stated. This approach provides some flexibility regarding the expensive initial gas calibration/verification, which can be difficult to implement due to the absence of appropriate flow calibration facilities.

### 4. CORIOLIS MASS FLOWMETERS AND LOW REYNOLDS NUMBER APPLICATIONS

The Reynolds number ( $Re$ ), one of the most important dimensionless numbers of fluid mechanics, accounts for the relationship between the inertial and viscous forces acting in a fluid transport application. As reported in Miller et al. [3] and Mills [4], CMF performance is sensitive to low Reynolds number conditions. The complex interaction between Coriolis forces and shearing forces under low  $Re$  conditions can produce under-readings. This interaction, dominated by the viscous effect at that flow regime, results in a secondary induced oscillatory force which is a function of the  $Re$ , as discussed by Kumar et al. [5].

This low Reynolds dynamic condition is driven by highly viscous fluids. The knowledge of the flow stream  $Re$  in the meter is relevant to compensate this effect. Coriolis mass flowmeters used in this work determine the  $Re$  number values dynamically, since the fluid viscosity is also estimated, thus, the low Reynolds number effect is compensated. The algorithm involved in this compensation is patented by Endress+Hauser Flowtec AG. This compensation technique has been shown to be effective for addressing the effects of low Reynolds on Coriolis meters by independent notified bodies, such as NMi Certin B.V. [6], to a level to be compliant with OIML R 117 [8].

### 5. CALIBRATION ROUND OF CORIOLIS MASS FLOWMETERS USING GAS AND VISCOS FLUIDS

The goal of this calibration round, using gas and viscous fluids as calibration fluids, is to prove that the tested flowmeters have an equal or better performance than the maximum permissible error (MPE) stated in the corresponding standard document, without adjustments in the CALF obtained in the initial water calibration. A summary of these calibration results is shown in Table 1.

A first group of calibrations carried out in Pigsar facilities (Germany's national standard for high-pressure natural gas metering) on a Promass F DN25 and a Promass Q DN25 is shown in Annex 1. The calibration fluid was natural gas at densities between  $17 \text{ kg/m}^3$  and  $40 \text{ kg/m}^3$ , measured under laboratory conditions and reported in the calibration certificate.

The deviations throughout the complete calibration range, as well as the instrument contributions to the measurement uncertainty ( $U_{\text{meter}} (95\%)$ ) and the total measurement uncertainty ( $U_{\text{tot}} (k=2)$ ) of the calibrations, are shown in Table 1. The maximum deviation values remained within the OIML R 137 MPE for Accuracy Class 1.0. This confirms the validity of the extension of the CALF obtained in water and applied to this gas application.

Another group of calibrations was carried out on a Promass Q DN80 in DNV (Det Norske Veritas, Groningen) flow facilities, this time using hydrogen at 30 bar and 40 bar and nitrogen at 2.3 bar, see Annex 2. This flowmeter was also initially calibrated with water with  $\pm 0.05\%$  o.r. of the maximum permissible error. The error (deviation) during the gas calibrations, the uncertainty of the repeatability, and the expanded measurement uncertainty are shown in Table 1 and in Annex 2.

As shown in Figure 2, the "as-found" gas calibrations were carried out at low mass flow rates, between 1.3 % and 4 %, relative to the maximum calibrated flow rate in water. An additional challenging condition was the low gas density, ranging from  $2.3 \text{ kg/m}^3$  to  $3.13 \text{ kg/m}^3$ , a common scenario in hydrogen

Table 1. Summary of the results of liquid and gas calibration for Coriolis mass flowmeters.

	Fluid	Calibration flow range kg/h	Turndown ratio	Density kg/m <sup>3</sup>	Pressure bar	Temp. °C	Max. Deviation %	Max. $U_{\text{meter}(95\%)}\%$	Max. $U_{\text{tot}(k=2)}\%$	Calibration facility
Promass F DN25 (Annex 1)	CH <sub>4</sub>	84 – 2800	33:1	17.0	21.2	17.0	-0.18	0.12	0.28	Pigsar
Promass Q DN25 (Annex 1)	CH <sub>4</sub>	84 – 2800	33:1	17.0	21.2	17.0	-0.17	0.19	0.30	Pigsar
Promass F DN80 (Annex 1)	CH <sub>4</sub>	2824 – 26804	10:1	24.3	30.1	21.0	0.41	0.43	0.49	Pigsar
Promass Q DN80 (Annex 2)	H <sub>2</sub>	455 – 746	1.6:1	2.36	30.2	33.0	0.25	0.23	0.42	DNV
	N <sub>2</sub>	493 – 1091	2.2:1	2.56	2.3	33.0	0.23	0.16	0.57	DNV
	H <sub>2</sub>	466 – 1337	2.9:1	3.13	40.0	33.0	0.39	0.14	0.38	DNV
Promass Q DN200 (Annex 2)	CH <sub>4</sub>	2400 – 70000	29:1	16.3	20	20.0	-0.11	0.14	0.27	Pigsar
Promass Q DN80	Sipitech 132 cSt	8665 – 117816	14:1	868.72	2.5	22.0	-0.32	0.01	0.25	NEL
Promass Q DN100	CO <sub>2</sub> 98% 32 bar	1764 – 45068	26:1	72.5	32	20.0	0.19	0.20	0.28	DNV
	CO <sub>2</sub> 98% 16 bar	890 – 22300	26:1	32.1	16	21.0	-0.66	0.22	0.28	DNV
	CO <sub>2</sub> 99% 16 bar	896 – 22600	25:1	39.2	16	-25.5	-0.19	0.23	0.28	DNV

applications. The composition and density of all fluids were measured under laboratory conditions and reported in the calibration certificate.

Even in this region of the flowmeter range, where the influence of the zero point stability is relevant, the error values obtained during the calibration were within the band of the maximum measured error (dashed line) for gas fluids at these flow rates in the non-linear region. It is also worth remarking that most of the error values were within the maximum measured error value specified in the instrument's technical information for gas flow measurement in the linear region ( $\pm 0.25\% \text{ o.r.}$ ).

Figure 3 shows the calibration carried out on a large diameter (DN200) Coriolis mass flowmeter Promass Q. This device was included to extend the diversity of the instruments already tested, ranging from DN25 and DN80 to larger sizes, but using the same approach, starting by water calibration at factory conditions where the CALF is determined, and then calibrating the instrument without adjustments with alternative fluids, in this case natural gas in Pigsar.

The error curves in Figure 3 combine natural gas (see Annex 2) and water calibration results of the Promass Q DN200. The initial calibration in water was carried out at two points, 57698 kg/h and 229184 kg/h, with  $\pm 0.1\% \text{ o.r.}$  as the tolerance limit, and an expanded measurement uncertainty,  $U$  ( $k = 2$ ), equal to 0.054 %. The results of the second calibration show a good agreement between both calibrations and the validity of the CALF obtained during the water calibration. The maximum error obtained in this calibration was -0.11 % (at the lowest flow rate) with a maximum  $U_{\text{meter}}$  (uncertainty of repeatability) of 0.14 %.

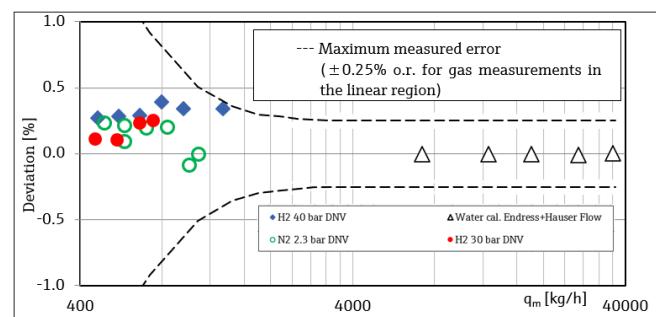


Figure 2. Promass Q DN80 errors, measuring H<sub>2</sub>, N<sub>2</sub> (DNV) and in its initial calibration with water.

This gas calibration, as Figure 3 shows, was covering only the low region of the water calibration range, however, the results are consistently good. This performance is possible because of the instrument's high zero point stability, repeatability, and linearity, also shown under gas measurement conditions.

Another group of calibrations reported are the results obtained in NEL (National Engineering Laboratories, Glasgow). A Promass F DN80 was calibrated with nitrogen, light mineral oils, and white oil Sipitech 132 cSt. The latter, shown in Table 1 and in Figure 4, was intended to evaluate the effectiveness of the low Reynolds compensation algorithms.

The low Reynolds compensation is a permanent feature in Promass flowmeters, but in this case, it was deactivated, Figure 4 (a), and activated, Figure 4 (b), to show the difference between the compensated and uncompensated measurement results. Error values shown in Figure 4 (b) confirm the capability of this feature to reduce the effects of the hydrodynamic conditions characterised by its low Reynolds number. Error values mainly remained better than  $\pm 0.2\%$ ; two points at very low flow were higher than  $\pm 0.2\%$  (-0.29 % and -0.32 %).

A new group of calibrations was also carried out in DNV, but measuring CO<sub>2</sub> gas at ambient and low temperatures. CO<sub>2</sub> applications are complex and challenging mainly due to the fluid characteristics and its behaviour under real process conditions. For these measurements, a Promass Q DN100, originally calibrated in water, was used. These measurements, listed in Table 1, were carried out at ambient temperatures (ca. 20 °C) at high and medium pressure (32 bar and 16 bar, respectively) and at low temperatures (ca. -25 °C) at medium pressure (ca. 16 bar). Error values shown in Figure 5 represent a consistent performance for both ranges of temperatures. The maximum

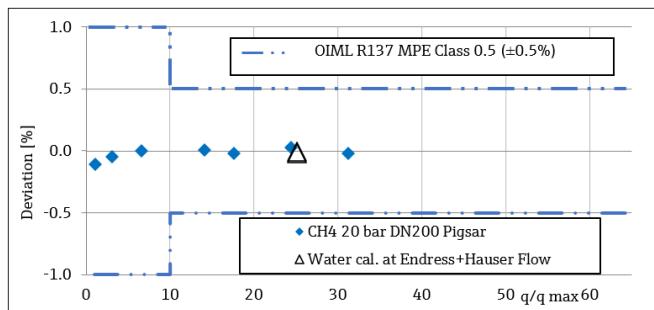


Figure 3. Promass Q DN200 errors, measuring CH<sub>4</sub> (Pigsar) with initial calibration with water.

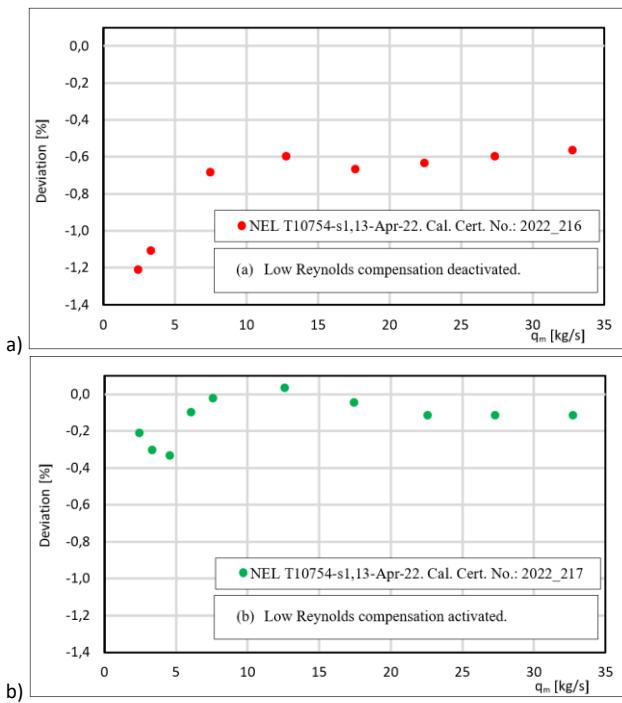


Figure 4. a) Promass F DN80 measuring Siptech 132 cSt, without Low  $Re$  compensation and b) Promass F DN80 measuring Siptech 132 cSt with Low  $Re$  compensation.

error value obtained (-0.66 %) occurred at a very low flow range under the influence of the zero point. The flowmeter proved to be insensitive to these changes of process conditions and fluid properties. These results qualify the meter OIML R137 Class 0.5 ( $\pm 0.5 \%$ ).

Figure 6 shows the general accordance of the measurement deviations (gas fluids) vs. the Reynolds number. The error values can also be compared against the indicated MPE of  $\pm 1 \%$  and  $\pm 0.5 \%$ , according to OIML R 137 [7], Classes 1 and 0.5, respectively. The obtained values remained within the acceptable error range throughout the entire range of the Reynolds number. All the gas measurements, except  $CO_2$  @ 16 bar, overperformed, staying within the band of error of  $\pm 0.5 \%$  (OIML R 137 Class 0.5), considering that these flowmeters are currently approved according to Class 1.

The combination of high zero point stability with high repeatability and linearity, also at an extended turndown ratio (up to 33:1) shown by these instruments, allows to achieve good accordance throughout the calibrated ranges, between the calibration results in water, in gas, and in liquids other than water. Also, the compensations implemented to correct deviations associated with low Reynolds conditions helped to maintain the error within the expected limits even under these conditions.

This favourable behaviour reinforces, with experimental data, the transferability approach from water to gas and from water to viscous fluids addressed in this paper.

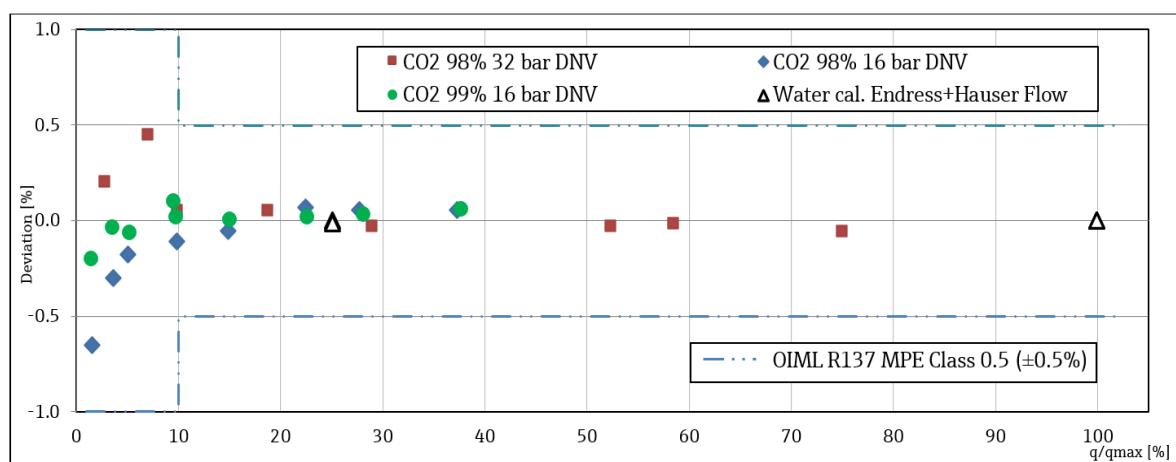


Figure 5. Promass F DN100 measuring  $CO_2$  at different pressures and compositions.

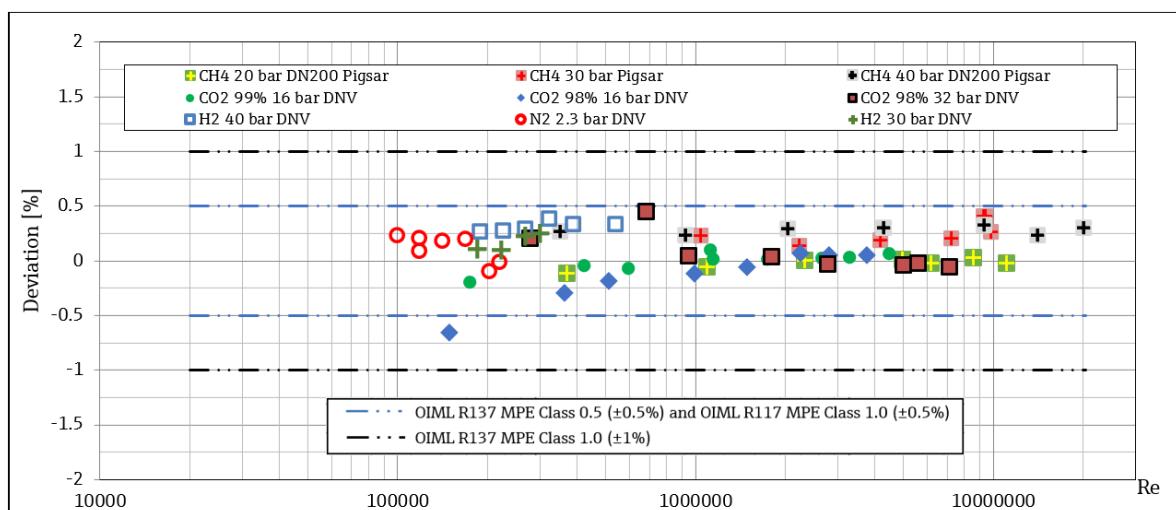


Figure 6. Deviations vs. Reynolds for five Coriolis mass flowmeters measuring different fluids (gas).

## 6. CONCLUSIONS

Coriolis mass flowmeters tested in this calibration round have consistently shown high performance in various gas and viscous fluids applications, using the same CALF obtained during their initial water calibration. Beyond the theoretical considerations, there are trustworthy results obtained in third-party calibration facilities with different sensors, different nominal diameters, pressures, fluids with different densities and viscosities, all of them initially calibrated using water and with no further adjustments.

These results are possible thanks to the design of the tested Coriolis mass flowmeters, which combines high zero point stability with high repeatability and linearity at an extended turndown ratio. In addition to that, the tested flowmeters are equipped with an algorithm to compensate the effect of the low Reynolds number condition, associated with high viscous fluids, as well as other corrections relevant for gases with low speed of sound and/or at high velocities.

These results also represent a reliable set of data to support and expand the concept of transferability for Coriolis mass flowmeters, sustaining the concept that their initial or subsequent water calibration can be valid when the meter is measuring energy-transition relevant fluids. This validity, which implies fulfilling the MPE values stated in custody transfer standards, such as OIML R 137 or OIML R 117, is considered by the notified bodies when granting the tested Coriolis mass flowmeters for custody transfer applications measuring liquid and gas.

## AUTHORS' CONTRIBUTION

Iryna Marfenko: writing – review & editing

Fabio O. Costa: formal analysis; data curation; validation

Douglas A. Garcia: writing – review & editing; data curation; visualisation;

Luiz O Pereira: funding acquisition

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## REFERENCES

- [1] ISO-4185, Measurement of liquid flow in closed conduits – Weighing method, 1980.
- [2] A. MPMS/AGA, API MPMS, Chapter 14.9/AGA Report No. 11: Measurement of Natural Gas by Coriolis Meter, 2013.
- [3] G. Miller, B. Belshaw, An investigation into the performance of Coriolis and ultrasonic meters at liquid viscosities up to 300 cSt, Int. North Sea Flow Measurement Workshop, 2008.
- [4] C. Mills, Coriolis questions, Bunkerspot, vol. 8, no. 1, 2011.
- [5] V. Kumar, M. Anklin, B. Schwenter, Fluid-structure interaction (FSI) simulations on the sensitivity of Coriolis flow meter under low Reynolds number flows, 15th Flow Measurement Conf. (FLOMEKO), Taipei, Taiwan, 13-15 October 2010. Online [Accessed 3 September 2025]  
<https://www.imeko.org/publications/tc9-2010/IMEKO-TC9-2010-077.pdf>
- [6] NMI-Certin\_BV, Evaluation Certificate Number TC7149, 2017 - 2023.
- [7] OIML, OIML R 137 Gas meters, 2012. Online [Accessed 10 September 2025]  
[https://www.oiml.org/en/files/pdf\\_r/r137-1-2-e12.pdf](https://www.oiml.org/en/files/pdf_r/r137-1-2-e12.pdf)
- [8] OIML, OIML R 117-2 , Dynamic measuring systems for liquids other than water, 2019. Online [Accessed 10 September 2025]  
[https://www.oiml.org/en/files/pdf\\_r/r117-p-e19.pdf/@@download/file/r117-p-e19.pdf](https://www.oiml.org/en/files/pdf_r/r117-p-e19.pdf/@@download/file/r117-p-e19.pdf)

## Annex 1:

Promass F DN25; 84 kg/h – 2800 kg/h CH<sub>4</sub> @ 20 bar



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Applicant		Coriolis meter Promass F				
Meter under Test	Type	Manufacturer	Serial number	Nominal Size	Year of manufacture	
		Endress+Hauser	S31AE202000	1"	2021	
<b>Test Conditions</b>	<b>Test medium</b>	Natural gas	CO <sub>2</sub>	1,57	mole %	
	Pressure, absolute	21,2 bar	H <sub>2</sub>	0,0	mole %	
	Gas Temperature	17 °C	Calorific value,s	10,35	kWh/m <sup>3</sup>	
	Gas density (p, T)	17,0 kg/m <sup>3</sup>	Density,normal	0,8306	kg/m <sup>3</sup>	
	Dyn. viscosity (p, T)	1,15E-5 Pa s	Normal conditions (273,15 K, 101,325 kPa)			
<b>Results</b> (as left)	Q <sub>i</sub> / Q <sub>max</sub>	Q <sub>i</sub> (kg/h)	Reynoldsnumber	Deviation (%)	n	U <sub>meter</sub> (%)
	0,03	82,77	0,10 *10 <sup>6</sup>	0,08	5	0,05
	0,05	128,17	0,16 *10 <sup>6</sup>	0,17	5	0,04
	0,10	282,89	0,35 *10 <sup>6</sup>	0,09	5	0,05
	0,21	600,77	0,74 *10 <sup>6</sup>	-0,06	5	0,03
	0,46	1296,39	1,61 *10 <sup>6</sup>	-0,12	6	0,12
	0,64	1794,62	2,22 *10 <sup>6</sup>	-0,18	5	0,08
	1,02	2843,55	3,48 *10 <sup>6</sup>	-0,03	5	0,12

Weighted mean error, with continuous and linear decrease of weighing factor between 0,7 Q<sub>max</sub> and Q<sub>max</sub>: -0,1 %.

The deviation is defined as:  $Deviation = \frac{(Indicated\ Value - Reference\ Value)}{(Reference\ Value)} \cdot 100\%$

where the reference volume refers to the conditions at the meter under test. The reported values of this deviation are the arithmetical means of n single repeat measurements at each flow-rate.

The reported total uncertainty is defined as:  $U_{tot} = \sqrt{U_{harmonized}^2 + U_{meter}^2}$

where  $U_{harmonized}$  is the expanded uncertainty of the harmonized reference value, stated as the standard uncertainty of measurement multiplied by the coverage factor k=2, and  $U_{meter}$  is the expanded standard uncertainty of the meter under test, determined on the base of n repeats at each flow-rate, multiplied by Student-t-factor (n) / n<sup>0,5</sup>, with a probability of 95%.

**Remarks** Security marks are applied

At customer's request the meter had not been adjusted.

The meter had been calibrated at 20 bar and at 40 bar.

The results at 40 bar are presented in certificate no. 19224/2021.

Following parameters have been used during the calibration and have an influence to the test results:

Measuring mode: Gas Stored zero(pip): 1,4  
Gas type: Methane Sensor pressure corr. (bar): 20  
Meter factor: 2,0496 Zero offset before calibration (g/3 min): 6,121  
Zero offset after calibration (g/3 min): 4,338

Tested in Dorsten at pigsar, on 2021-05-06 Göbbeler

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Promass Q DN25; 84 kg/h – 2800 kg/h CH<sub>4</sub> @ 20 bar



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Applicant		Coriolis meter Promass Q				
Meter under Test	Type	Manufacturer	Serial number	Nominal Size	Year of manufacture	
		Endress+Hauser	RBOF720200	1"	2020	
<b>Test Conditions</b>	<b>Test medium</b>	Natural gas	CO <sub>2</sub>	1,53	mole %	
	Pressure, absolute	21,2 bar	H <sub>2</sub>	0,0	mole %	
	Gas Temperature	17 °C	Calorific value,s	10,35	kWh/m <sup>3</sup>	
	Gas density (p, T)	17,0 kg/m <sup>3</sup>	Density,normal	0,8312	kg/m <sup>3</sup>	
	Dyn. viscosity (p, T)	1,15E-5 Pa s	Normal conditions (273,15 K, 101,325 kPa)			
<b>Results</b> (as left)	Q <sub>i</sub> / Q <sub>max</sub>	Q <sub>i</sub> (kg/h)	Reynoldsnumber	Deviation (%)	n	U <sub>meter</sub> (%)
	0,03	85,09	0,11 *10 <sup>6</sup>	-0,11	6	0,12
	0,05	132,83	0,16 *10 <sup>6</sup>	0,04	5	0,05
	0,10	281,18	0,35 *10 <sup>6</sup>	0,13	5	0,03
	0,22	602,46	0,74 *10 <sup>6</sup>	0,03	5	0,03
	0,46	1278,39	1,56 *10 <sup>6</sup>	-0,17	5	0,10
	0,64	1804,60	2,22 *10 <sup>6</sup>	-0,13	5	0,19
	0,98	2735,50	3,35 *10 <sup>6</sup>	-0,01	6	0,14

Weighted mean error, with continuous and linear decrease of weighing factor between 0,7 Q<sub>max</sub> and Q<sub>max</sub>: -0,08 %.

The deviation is defined as:  $Deviation = \frac{(Indicated\ Value - Reference\ Value)}{(Reference\ Value)} \cdot 100\%$

where the reference volume refers to the conditions at the meter under test. The reported values of this deviation are the arithmetical means of n single repeat measurements at each flow-rate.

The reported total uncertainty is defined as:  $U_{tot} = \sqrt{U_{harmonized}^2 + U_{meter}^2}$

where  $U_{harmonized}$  is the expanded uncertainty of the harmonized reference value, stated as the standard uncertainty of measurement multiplied by the coverage factor k=2, and  $U_{meter}$  is the expanded standard uncertainty of the meter under test, determined on the base of n repeats at each flow-rate, multiplied by Student-t-factor (n) / n<sup>0,5</sup>, with a probability of 95%.

**Remarks** Security marks are applied

At customer's request the meter had not been adjusted.

The meter had been calibrated at 20 bar and at 40 bar.

The results at 40 bar are presented in certificate no. 19224/2021.

Following parameters have been used during the calibration and have an influence to the test results:

Measuring mode: Gas Stored zero(pip): -43  
Gas type: Methane Sensor pressure corr. (bar): 20  
Meter factor: 0,83113 Zero offset before calibration (g/3 min): -5,281  
Zero offset after calibration (g/3 min): -0,151

Tested in Dorsten at pigsar, on 2021-04-23 Görgülü

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Promass F DN80; 2824 kg/h – 26804 kg/h CH<sub>4</sub> @ 30 bar



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Applicant		Coriolis meter Promass 300				
Meter under Test	Type	Manufacturer	Serial number	Nominal Size	Year of manufacture	
		Endress+Hauser	SA111F02000	3"	2021	
<b>Test Conditions</b>	<b>Test medium</b>	Natural gas	CO <sub>2</sub>	1,01	mole %	
	Pressure, absolute	30,1 bar	H <sub>2</sub>	0,0	mole %	
	Gas Temperature	21 °C	Calorific value,s	10,32	kWh/m <sup>3</sup>	
	Gas density (p, T)	24,3 kg/m <sup>3</sup>	Density,normal	0,8346	kg/m <sup>3</sup>	
	Dyn. viscosity (p, T)	1,20E-5 Pa s	Normal conditions (273,15 K, 101,325 kPa)			
<b>Results</b> (as left)	Q <sub>i</sub> / Q <sub>max</sub>	Q <sub>i</sub> (kg/h)	Reynoldsnumber	Deviation (%)	n	U <sub>meter</sub> (%)
	0,10	2824,10	1,04 *10 <sup>6</sup>	-0,23	4	0,05
	0,22	6072,58	2,23 *10 <sup>6</sup>	0,14	3	0,04
	0,42	11322,56	4,16 *10 <sup>6</sup>	0,19	3	0,09
	0,72	19613,22	7,22 *10 <sup>6</sup>	0,21	3	0,11
	0,93	25267,73	9,32 *10 <sup>6</sup>	0,41	6	0,13
	0,95	25615,65	9,44 *10 <sup>6</sup>	0,41	5	0,43
	0,99	26804,30	9,88 *10 <sup>6</sup>	0,27	6	0,30

Weighted mean error, with continuous and linear decrease of weighing factor between 0,7 Q<sub>max</sub> and Q<sub>max</sub>: 0,28 %.

The deviation is defined as:  $Deviation = \frac{(Indicated\ Value - Reference\ Value)}{(Reference\ Value)} \cdot 100\%$

where the reference volume refers to the conditions at the meter under test. The reported values of this deviation are the arithmetical means of n single repeat measurements at each flow-rate.

The reported total uncertainty is defined as:  $U_{tot} = \sqrt{U_{harmonized}^2 + U_{meter}^2}$

where  $U_{harmonized}$  is the expanded uncertainty of the harmonized reference value, stated as the standard uncertainty of measurement multiplied by the coverage factor k=2, and  $U_{meter}$  is the expanded standard uncertainty of the meter under test, determined on the base of n repeats at each flow-rate, multiplied by Student-t-factor (n) / n<sup>0,5</sup>, with a probability of 95%.

**Remarks** Security marks are applied

At customer's request the meter had not been adjusted.

Tested in Dorsten at pigsar, on 2022-09-09 Göbbeler

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